

1 **Effect of solvent on nanoparticle production of  $\beta$ -carotene by a**  
2 **supercritical anti-solvent process**

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23 **ABSTRACT**

24 Production of micro- to nano-sized particles of  $\beta$ -carotene was investigated using the  
25 solution-enhanced dispersion by supercritical fluids (SEDS) process.  $\beta$ -Carotene was  
26 dissolved in dichloromethane (DCM), *n,n*-dimethylformamide (DMF), *n*-hexane, or ethyl  
27 acetate, and supercritical CO<sub>2</sub> was used as an anti-solvent. The effects of the organic solvent,  
28 operating pressure, and temperature were examined. The morphologies of the particles  
29 produced by the SEDS were observed by field emission-scanning electron microscopy and  
30 particle sizes were determined by image analysis. Irregularly shaped micro particles were  
31 produced in the system which uses DCM and DMF solution. Plate-like micro particles were  
32 produced by using *n*-hexane solution, and irregular nanoparticles were produced by using  
33 ethyl acetate solution. The optimum operating conditions were determined to be ethyl acetate  
34 as solvent operated at 8–12 MPa and 40–60 °C.

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36 **Keywords:**  $\beta$ -Carotene; Nanoparticle formation; Supercritical anti-solvent, Supercritical  
37 CO<sub>2</sub>

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39 **1. INTRODUCTION**

40 Carotenoids pigments, found in plants and some other photosynthetic organisms, consist  
41 of eight isoprene units joined in a head-to-tail pattern, and have highly vivid colours. The  
42 main function of carotenoids in plants is the removal of active oxygen generated by various  
43 bioreactions [1]. Carotenoids are widely used as high-quality natural colorants in the food,  
44 cosmetic, and nutraceutical industries [2]. It is also used in dietary supplements because it  
45 exhibits many functionalities such as an inhibitory effect for several types of cancer,

46 including lung and mammary cancers and leukaemia, in addition to antioxidant activities [3–  
47 5]. Industrial carotenoids are usually crystalline powders that are soluble in oils and organic  
48 solvents, and they have low water solubilities [6,7].  $\beta$ -Carotene is one of the most common  
49 carotenoid pigments used in the industries. The physicochemical properties of  $\beta$ -carotene  
50 are shown in **Table 1** [8]. Micronized  $\beta$ -carotene particles are more effective for human  
51 nutrition, since micronization increases the  $\beta$ -carotene concentration in the serum and lymph.  
52 The miniaturization of carotenoid particles may enhance the bioavailability, without causing  
53 excessive their accumulation in the body [9].

54 Fine particle formation using supercritical carbon dioxide (SC-CO<sub>2</sub>) has recently attracted  
55 attention. Since CO<sub>2</sub> has low critical temperature, it may be suitable for heat-sensitive  
56 materials. Additionally, SC-CO<sub>2</sub> can be easily separated from the produced particles along  
57 with the organic solvent as SC-CO<sub>2</sub> again becomes the gas phase at ambient temperature and  
58 pressure. The supercritical anti-solvent (SAS) process is one of the micronization methods  
59 that can be applied for making fine particles from various materials such as pharmaceutical  
60 and cosmetic materials and pigments [10–15]. In a typical SAS process, a solution containing  
61 compounds to be processed and an organic solvent are fed via a nozzle into a precipitator to  
62 produce particles filled with SC-CO<sub>2</sub>. Supersaturation was caused by mixing of the solution  
63 with SC-CO<sub>2</sub> in the precipitator, leading to crystal nucleation and growth. Several factors  
64 affect the particle size and morphology, such as operating temperature, pressure, CO<sub>2</sub> and  
65 solution flow rate, kind of organic solvent, and the nozzle type and its inner diameter [15–  
66 23].

67 The solution-enhanced dispersion by supercritical fluids (SEDS) process is one of the  
68 modified SAS processes. In this process, the solution and SC-CO<sub>2</sub> are sprayed into a  
69 precipitator by a coaxial nozzle [11,24–28]

70 Water-soluble nanoparticles of the carotenoid/cyclodextrin complex were produced for  
71 synthesizing medicines by the SEDS process [29]. In this study, the organic solvent used  
72 was *n,n*-dimethylformamide (DMF), which is not approved anywhere in the world for use  
73 in food or supplement products. In this work, fine particle production of  $\beta$ -carotene with  
74 some organic solvents that are approved as food additives has been investigated for  
75 application to food products. The most appropriate solvent was selected from *n*-hexane, ethyl  
76 acetate, dichloromethane (DCM), and DMF. The effects of operating pressure and  
77 temperature of the process on the size and shape of the obtained particles were examined.  
78 The SEDS process was carried out in a semi-continuous cell at 8–12 MPa and 40–60 °C.  
79 The morphology of the particles generated was observed by field emission-scanning electron  
80 microscopy (FE-SEM).

## 81 2. MATERIALS AND METHODS

### 82 2.1 *Materials and chemicals*

83  $\beta$ -Carotene (purity >80%), which was crushed mechanically, was purchased from Wako  
84 Pure Chemical Industries, Ltd., Japan. DCM (purity >99%), DMF (purity >99.5%), *n*-hexane  
85 (purity >95%), and ethyl acetate (purity 99.3%) were obtained from Kanto Chemical Co.,  
86 Inc., Japan. CO<sub>2</sub> (purity >99.5%) was supplied by Sogo Co., Japan.

### 87 2.2 *Equipment and procedures*

88 The SEDS process was carried out in a semi-continuous precipitation vessel. **Figure 1**  
89 shows a schematic diagram of the SEDS apparatus. The apparatus consists of a CO<sub>2</sub> chiller  
90 (Cooling Unit CLU-33, Iwaki Asahi Techno Glass, Tokyo, Japan), HPLC pumps for CO<sub>2</sub>  
91 and solution (PU-980 Intelligent HPLC pump, JASCO Co., Tokyo, Japan), a heating

92 chamber (Incubator EI-700B, AS ONE Co, Osaka, Japan), a precipitation vessel (SUS316  
93 cell, inner diameter: 3 cm, length: 17 cm, volume: 120 cm<sup>3</sup>, maximum design pressure: 30  
94 MPa), a coaxial nozzle (**Fig. 2**, nozzle inner diameters: 2.4 and 0.8 mm, inner diameter of  
95 the nozzle outlet: 0.4 mm, custom-made by Taiatsu Techno Co., Tokyo, Japan), a wet gas  
96 meter for CO<sub>2</sub> flow rate (Sinagawa Co., Tokyo, Japan), a membrane filter for collecting  
97 particles (100 nm PTFE membrane filter, Advantec, Tokyo, Japan) placed inside a Swagelok  
98 filter housing, and a back-pressure regulator (AKICO Co., Tokyo, Japan).

99 Experiments on the SEDS process were carried out as follows: liquefied CO<sub>2</sub> was introduced  
100 into the system using an HPLC pump (-5 °C and operating pressure) at a constant flow rate.  
101 The CO<sub>2</sub> was heated in the preheater, placed in heating chamber, to change it to the  
102 supercritical state. When the temperature and pressure in the system reached the desired  
103 operating conditions, β-carotene dissolved in the organic solvent (1.5 mg/mL) was pumped  
104 using an HPLC pump (at the operating temperature and pressure) at the desired flow rate.  
105 SC-CO<sub>2</sub> and the β-carotene solution were mixed and introduced into the precipitator via the  
106 coaxial nozzle. β-Carotene was precipitated by supersaturation by using the anti-solvent  
107 effect. After stopping the solution feed pump, the particles and the system line were washed  
108 with SC-CO<sub>2</sub> to help remove the organic solvent from the particles. Finally, particles were  
109 collected from the membrane filter after depressurization. The experiments were carried out  
110 at operating pressures 8–12 MPa and operating temperatures 40–60 °C. The concentration  
111 of β-carotene in the organic solvent (DCM, DMF, *n*-hexane, and ethyl acetate) was 1.5  
112 mg/mL. The flow rates of the solution and supercritical CO<sub>2</sub> were 0.25 and 20 mL/min (at  
113 the pump conditions), respectively. **Table 2** shows the detailed experimental conditions.

114

115 *2.3 Analysis and characterization*

116 The shape and surface characteristics of the raw materials and the SEDS-processed particles  
117 were observed using a FE-SEM (S-5200, Hitachi, Tokyo, Japan). The samples were sputter-  
118 coated with gold in a high-vacuum evaporator and examined using FE-SEM at 30 kV. The  
119 particle sizes and size distributions were measured using Image J software which was  
120 developed by the National Institutes of Health.

121

### 122 3. RESULTS AND DISCUSSION

#### 123 3.1 Selection of solvent

124 The suitability of the solvent in the SEDS process was tested at 12 MPa, 40 °C and  
125 concentration of 1.5 mg/mL for solvents, DCM, DMF, *n*-hexane, and ethyl acetate. **Table**  
126 **3** shows the physicochemical properties of these organic solvents from Chemical database  
127 by National Center for Manufacturing Sciences, USA and Showa Chemical Industry  
128 Co.,Ltd., Japan. The experiments showed that particles were obtained for all conditions;  
129 however, their size and morphology were different, depending on the solvent. **Figure 3**  
130 shows the SEM image of the raw material for  $\beta$ -carotene, which was crushed mechanically.  
131 **Figure 4** shows the SEM image of the particles produced by SEDS. The particle size of the  
132 raw material for  $\beta$ -carotene was 2–15  $\mu$ m. In the case of processing with DCM and DMF  
133 solution, irregular micro-particles were formed. On the other hand, plate-like micro-  
134 particles were generated by using *n*-hexane as the solvent. Irregular nanoparticles were  
135 precipitated by ethyl acetate solution, as shown in Fig. 4. The critical point of the binary  
136 system can be found from the phase equilibrium curve. **Figure 5** shows the phase  
137 compositions for the systems of CO<sub>2</sub> and DMF, DCM, *n*-hexane, and ethyl acetate,  
138 respectively, at 40 or 45 °C [30–33]. The maximum value of the four curves indicates a

139 critical point of the mixture of organic solvent and CO<sub>2</sub>. The critical point of the CO<sub>2</sub>+DMF  
140 system is at 9 MPa, while for all the other solvents it is near 8 MPa.

141 As seen in Fig. 5, for the pressure of 4 MPa condition, the compositions of the CO<sub>2</sub> and  
142 organic solvent systems were different for each type of solvent. The most soluble organic  
143 solvent was ethyl acetate, followed in the decreasing order by hexane, DCM, and DMF. The  
144 solubility is an important parameter in this process. The particle size is reduced by increasing  
145 the supersaturation levels. The supersaturation depends on the difference of  $\beta$ -carotene  
146 solubility between before and after the contact of the organic solvent with SC-CO<sub>2</sub>.

147 The characteristics of subcritical CO<sub>2</sub>, such as density, viscosity, diffusivity, and surface  
148 tension are quite different in the SC-CO<sub>2</sub> region [34]. The reason why the size and shape of  
149 the particles changed, depending on the kind of organic solvent used, is considered next. The  
150 effects of the SAS system on the solubility of the three-component system comprising  $\beta$ -  
151 carotene, CO<sub>2</sub>, and organic solvent should be evaluated. However, because there is no data  
152 available on this three-component system and the calculation process would be highly  
153 complicated, this system has been discussed by using solubility parameters [37-38] and  
154 experimentally obtained solubility data of  $\beta$ -carotene in various organic solvents [37]. **Table**  
155 **4** shows the Hansen solubility parameters of  $\beta$ -carotene and organic solvents. Additionally,  
156 Hansen solubility parameters of CO<sub>2</sub> at various temperature and pressure conditions were  
157 calculated by King; for the 40 °C and 12 MPa condition, the total solubility parameter of  
158 CO<sub>2</sub> was about 10 [38]. Hansen solubility parameters are used to predict the solubility of a  
159 substance based on the following concept: two substances are easily soluble with each other  
160 when the molecules of the respective substances exhibit similar interactions. Hansen  
161 solubility parameters consist of three parameters,  $\delta_d$ ,  $\delta_p$ , and  $\delta_h$ , which denote the dispersion,  
162 polar, and hydrogen bonding interactions, respectively. When the parameters of two

163 components are located near each other in the Hansen space, it means that the two molecules  
164 will easily dissolve into each other.

165

166 The total Hansen solubility parameter can be calculated using Eq. (1)

$$167 \quad (\delta_t)^2 = (\delta_d)^2 + (\delta_p)^2 + (\delta_h)^2 \quad (1)$$

168

169 Where  $\delta_t$  is the total solubility parameter,  $\delta_d$  is the dispersion solubility parameter,  $\delta_p$  is the  
170 polar solubility parameter, and  $\delta_h$  is the hydrogen bonding solubility parameter [35].

171 The SEDS process is related to both equilibria and transport phenomena. Although  
172 transport phenomena are important factor which influences the particle morphology, we  
173 focus on the equilibria factor to discuss the effect of solvent. The total solubility parameter,  
174  $\delta_t$  of ethyl acetate is closest to that of  $\beta$ -carotene among the solvent used in this work,  
175 although tendency of solubility of  $\beta$ -carotene in organic solvent is different from that of the  
176 solubility parameter as shown in **Table 5**. In SEDS process, the solubility of the carotenoid  
177 in organic solvent is very important and also complicated parameter. When the solubility of  
178 carotenoid in the solvent is too high, crystal generation is suppressed because of reduced  
179 anti-solvent power. When organic solvent has a certain level of solubility of carotenoid,  
180 crystal generation and growth occur easily by contact with the SC-CO<sub>2</sub> as anti-solvent.  
181 Therefore, it is desirable to use an organic solvent which have suitable balance of the  
182 solubility for both SC-CO<sub>2</sub> and carotenoids. In the case of ethyl acetate system, smaller  
183 uniform particles were obtained. Consequently, it is considered that ethyl acetate has the  
184 most suitable solubility balance with SC-CO<sub>2</sub> and  $\beta$ -carotene compared to the other solvents  
185 such as DCM, DMF and n-hexane. The morphology of the  $\beta$ -carotene particles was also  
186 quite different, depending on the organic solvent, probably because polymorphic crystals are  
187 affected by the solvent in which they were dissolved [39].



188

### 189 3.2 *Effect of pressure and temperature*

190 The effects of pressure and temperature on the morphology and size of the treated particles  
191 were studied at constant concentrations of  $\beta$ -carotene in the ethyl acetate solution. The effect  
192 of pressure was considered in the pressure range 8–12 MPa and at a constant temperature of  
193 40 °C. The particle sizes decrease with increasing pressure as shown in **Fig. 6**. This trend  
194 has also been observed in a previous work [29]. When the process was carried out at a lower  
195 pressure, the particles tended to be larger and plate-like. However, as the pressure increased,  
196 irregularly shaped nanoparticles were obtained. The smallest particles (diameter of around  
197 135 nm) were formed at 10-12 MPa and 40 °C. This decrease in the particle size with  
198 increasing pressure can be explained by the rate of SC-CO<sub>2</sub> diffusion into the organic solvent  
199 droplets that is dependent on the operation pressure [40]. The solubility of the solvent in SC-  
200 CO<sub>2</sub> increases at higher pressures [41–43]. Moreover, the droplet size will also decrease with  
201 an increase in the SC-CO<sub>2</sub> density, and reduces the interfacial tension between SC-CO<sub>2</sub> and  
202 the solvent at higher pressures. This leads to SC-CO<sub>2</sub> diffusing into the solvent immediately  
203 when the pressure increases. The partial molar volume and cohesive energy density of the  
204 organic solvent will decrease due to an increase in the diffusive driving force. Therefore, the  
205 higher supersaturation of the carotenoid in the solvent is caused by a higher mass transfer  
206 rate and a higher solubility of the solvent in SC-CO<sub>2</sub>. Therefore, the solvent power of the  
207 organic solvent for the solute decreases rapidly, causing the particle to become smaller [40].

208 The experiments were also carried out at various temperatures: 40, 50, and 60 °C, at a  
209 pressure of 12 MPa. Particle size increased with increasing temperature as shown in **Fig. 7**.  
210 The smallest particles, with a diameter of around 135 nm, were formed at 40 °C and 12 MPa.  
211 Higher temperatures reduced the CO<sub>2</sub> density, forming larger droplets. Therefore, a lower

212 CO<sub>2</sub> density leads to a higher solvent power for the solute, and it causes a lower mass transfer  
213 rate and lower supersaturation of solute in the organic solvent [40]. This explains why the  
214 particles sizes were reduced at lower temperatures. Therefore, the smallest particles of  $\beta$ -  
215 carotene were formed at above the critical pressure (10–12 MPa) and at the lowest  
216 temperature (40 °C), because the ethyl acetate solution immediately became supersaturated  
217 under these conditions [16,31,44].

218

#### 219 **4. CONCLUSION**

220

221 Nano-particles of  $\beta$ -carotene were successfully produced by the SEDS process. The effects  
222 of parameters such as the kind of organic solvent, operating pressure, and temperature on  
223 the particle morphology and size were investigated. Irregularly formed micro-particles (5 to  
224 20  $\mu\text{m}$ ) were precipitated when processing with DCM and DMF solution. Plate-like micro-  
225 particles (10 to 20  $\mu\text{m}$ ) were generated by using *n*-hexane as the solvent. Irregularly formed  
226 nanoparticles (135 nm) were precipitate by using ethyl acetate solution. The reduction of  $\beta$ -  
227 carotene particle size from 10  $\mu\text{m}$  to 135 nm by increasing pressure was observed. And  
228 particles size of  $\beta$ -carotene were changed from 135 nm to 10 mm by increasing temperature.  
229 Optimum conditions for fine particle production (135 nm mean size) were found this work  
230 to be 12 MPa and 40 °C and using ethyl acetate as organic solvent.

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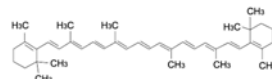
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325 **Tables with headings**

326

327 **Table 1.** Physicochemical properties of  $\beta$ -carotene (Source: Skeget et al., 1997)

	Formula	Molecular weight	Melting point (°C)	Critical point
$\beta$ -Carotene	$C_{40}H_{56}$ 	536.87	172–173	1212.42 °C 799.3 MPa

328

329 **Table 2.** Experimental conditions (Concentration of 1.5 mg/mL, liquefied CO<sub>2</sub> flow rate of

330 20 mL/min, solution flow rate of 0.25mL/min)

Sample No.	Solvent	Pressure (MPa)	Temperature (°C)
1	<i>n</i> -Hexane	12	40
2	Ethyl acetate	12	40
3	DCM	12	40
4	DMF	12	40
5	Ethyl acetate	8	40
6	Ethyl acetate	10	40
7	Ethyl acetate	12	50
8	Ethyl acetate	12	60

DCM; dichloromethane, DMF; *n,n*-dimethylformamide

331

332 **Table 3.** Physicochemical properties of organic solvents (Source: Chemical database by

333 NCMS and Showa Chemical Co., Ltd)

	Formula	Molecular weight (g/mol)	Melting point (°C)	Boiling point (°C)
<i>n</i> -Hexane	$C_6H_{14}$	86.18	-95	69
Ethyl acetate	$C_4H_8O_2$	88.11	-83.6	77
DCM	$CH_2Cl_2$	84.93	-96.7	39.8
DMF	$C_3H_7NO$	73.09	-61	153

DCM: dichloromethane, DMF: *n,n*-dimethylformamide.

334

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336

337 **Table 4.** Hansen solubility parameters of  $\beta$ -carotene and organic solvents

	Solubility parameter (MPa <sup>1/2</sup> )			
	$\delta_d$	$\delta_p$	$\delta_h$	$\delta_t$
$\beta$ -Carotene (25 °C)	17.1	2.39	5.54	18.0
<i>n</i> -Hexane (RT)	14.9	0	0	14.9
Ethyl acetate (RT)	15.8	5.3	7.2	18.1
DCM (RT)	18.2	6.3	6.1	20.2
DMF (RT)	17.4	13.7	11.3	24.9

$\delta_d$ : Dispersion solubility parameter,  $\delta_p$ : Polar solubility parameter,  $\delta_h$ : Hydrogen bonding solubility parameter,  $\delta_t$ : Total solubility parameter, RT: Room temperature, DCM: dichloromethane, DMF: *n,n*-dimethylformamide

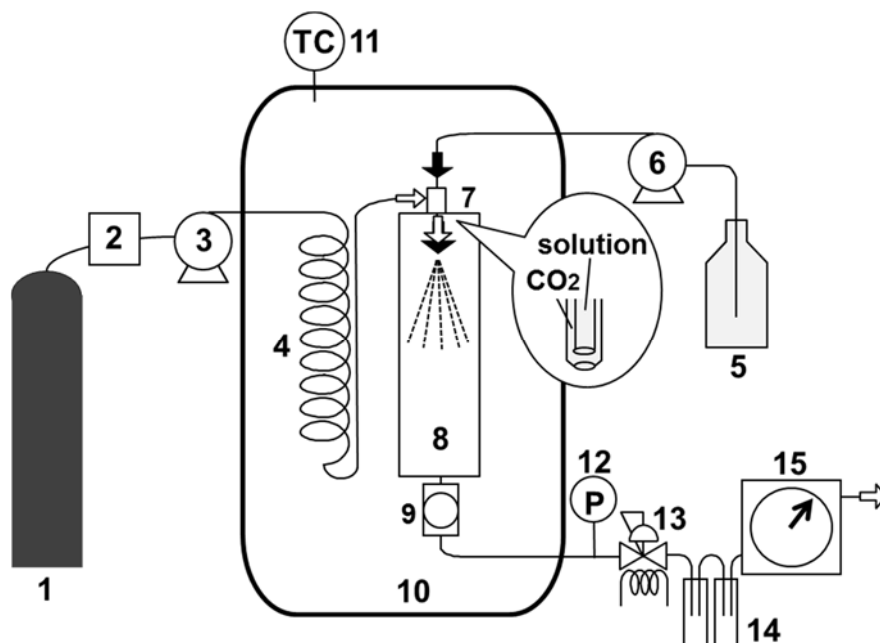
338

339 **Table 5.** Solubility of  $\beta$ -carotene in organic solvents (Source: Craft et al., 1992)

Organic solvent	Solubility [mg/L]
<i>n</i> -Hexane	600
Ethyl acetate	500
DCM	6000
DMF	200

340 DCM: dichloromethane, DMF: *n,n*-dimethylformamide

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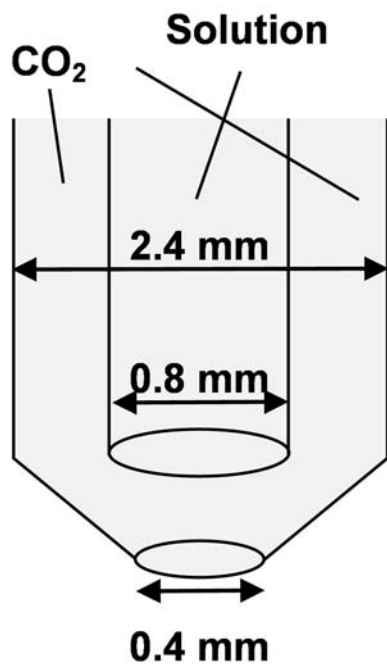


342

343 **Figure. 1:** Schematic diagram of the SEDS process. (1) CO<sub>2</sub> cylinder, (2) chiller, (3) CO<sub>2</sub>  
 344 pump, (4) CO<sub>2</sub> pre-heater, (5) carotenoid solution, (6) feed pump, (7) coaxial nozzle, (8)  
 345 precipitator, (9) membrane filter placed in Swagelok filter, (10) heating chamber, (11)  
 346 temperature controller, (12) pressure gauge, (13) back-pressure regulator, (14) trap, and (15)  
 347 wet gas meter. (<sup>1</sup>SEDS: Solution enhanced dispersion by supercritical fluids)

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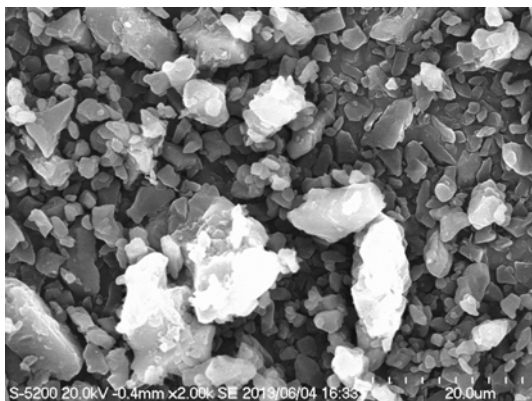




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350 **Figure. 2:** Schematic diagram of the coaxial nozzle.

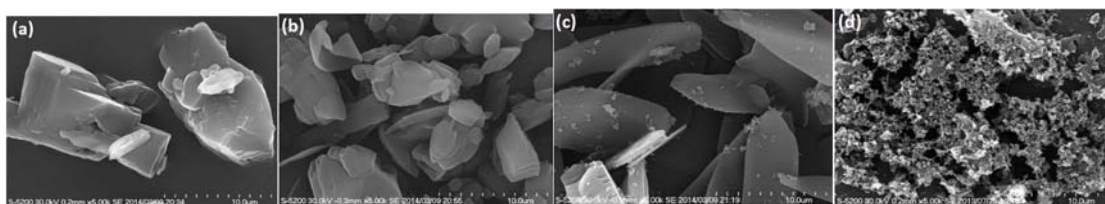
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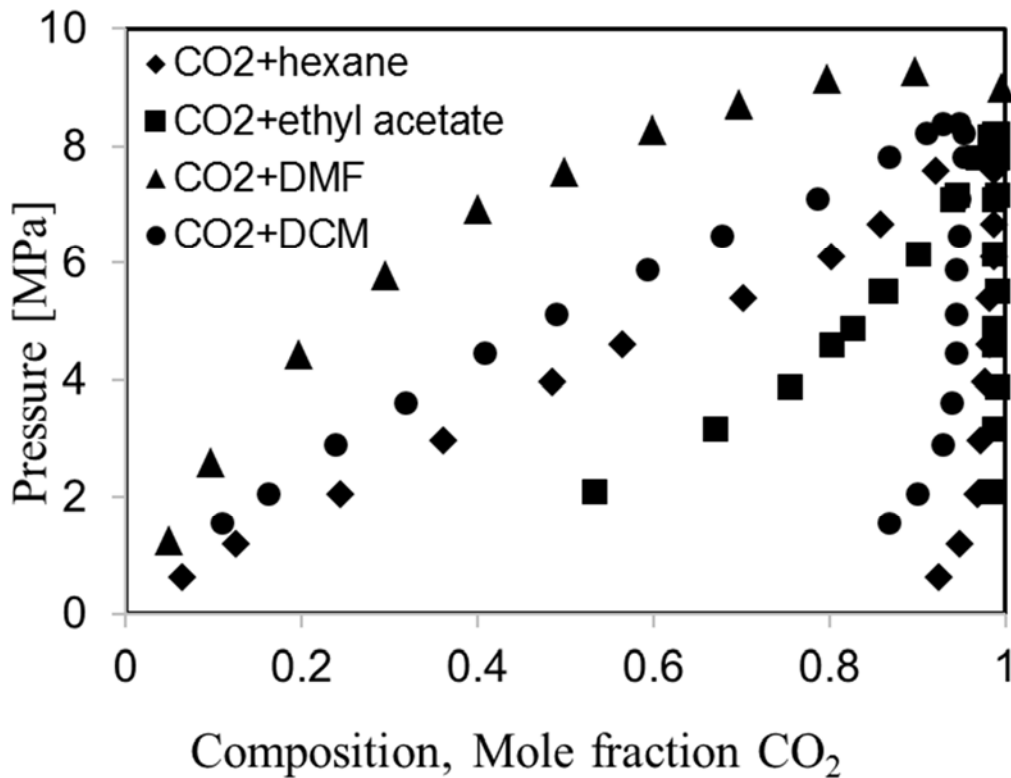
353 **Figure. 3:** SEM image of the raw material for the  $\beta$ -carotene crystal.

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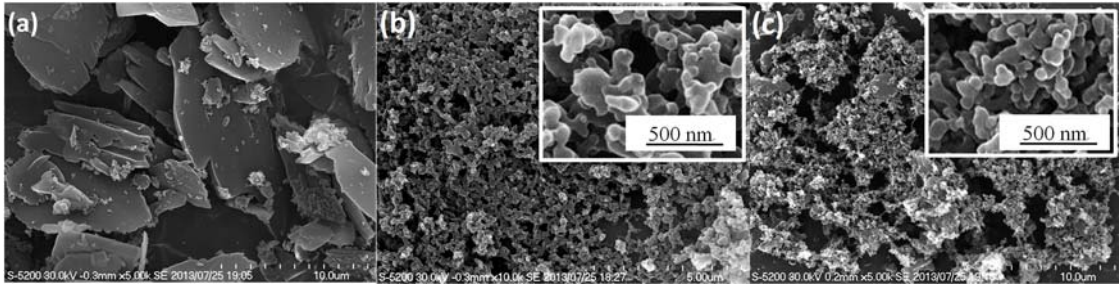


355

356 **Figure. 4:** SEM image of  $\beta$ -carotene particles treated with various solvents ((a)  
 357 dichloromethane, (b) *N,N*-dimethylformamide, (c) *n*-hexane and (d) ethyl acetate) under the  
 358 following conditions: temperature, 40 °C; pressure, 12 MPa;  $1\text{CO}_2$  flow rate, 20 mL/min;  
 359 solution flow rate, 0.25 mL/min; and concentration, 1.5 mg/m.  
 360



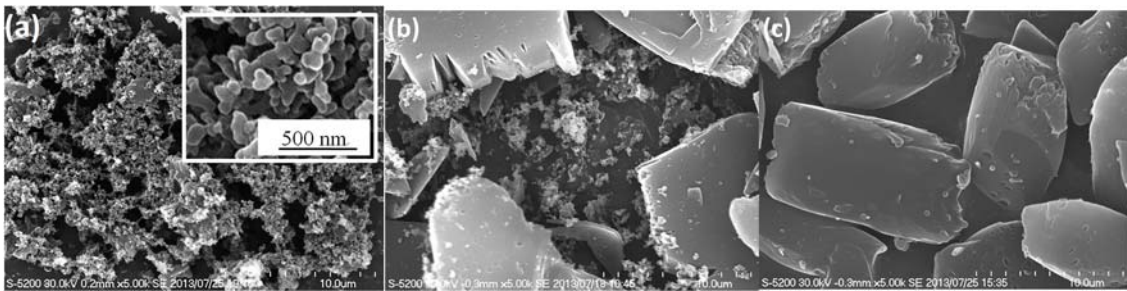
362 **Figure. 5:** Phase composition for the system of  $\text{CO}_2$  with *N,N*-dimethylformamide (DMF)  
 363 (40 °C), dichloromethane (DCM) (45 °C), *n*-hexane (40 °C), and ethyl acetate (40 °C), using  
 364 reported experimental data (Ohgaki et al., 1976; Wagner et al., 1994; Temtem et al., 2006;  
 365 Tsivintzelis et al., 2004).  
 366



367

368 **Figure. 6:** SEM image of treated particles precipitated from an ethyl acetate solution of  $\beta$ -  
369 carotene (1.5 mg/mL) under the following conditions: temperature, 40 °C; CO<sub>2</sub> flow rate, 20  
370 mL/min; solution flow rate, 0.5 mL/min; and various pressures ((a) 8 MPa, (b) 10 MPa and  
371 (c)12 MPa).

372



373

374 **Figure. 7:** SEM image of treated particles precipitated from an ethyl acetate solution of  $\beta$ -  
375 carotene (1.5 mg/mL) under the following conditions: pressure, 12 MPa; CO<sub>2</sub> flow rate, 20  
376 mL/min; solution flow rate, 0.5 mL/min; and various temperatures ((a) 40 °C, (b) 50 °C and  
377 (c) 60 °C).

378

**Type of Article:** Table of Contents text.

- Micro- to nano-sized particles of beta-carotene were produced by SEDS.
- Ethyl acetate was a more suitable solvent than DCM, DMF, and hexane for the process.
- Nano-particles were obtained with an ethyl acetate solution at 40 °C and 10-12 MPa.

**Title**

Effect of solvent on nanoparticle production of  $\beta$ -carotene by a supercritical anti-solvent process

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